



Conversion of passive sampling data into concentrations in the sampled media

NORMAN expert group meeting
Prague, 27th May 2009



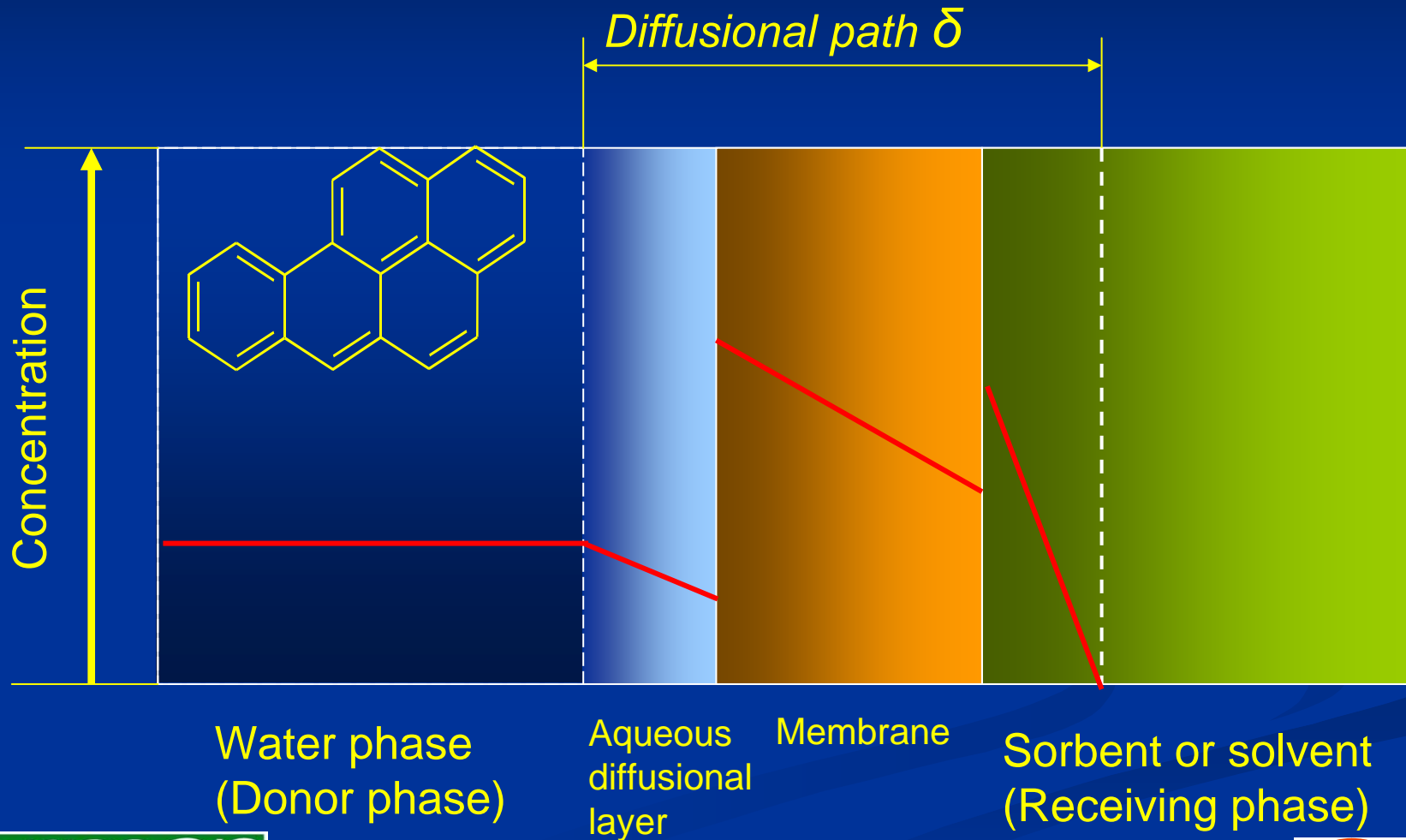
Existing passive sampling techniques

- Sub areas:
 - **hydrophobic** organic compounds, e.g. POPs
 - **polar** (hydrophilic) organic compounds such as pharmaceuticals, polar pesticides and illicit drugs
 - **trace metals and organometallic** compounds

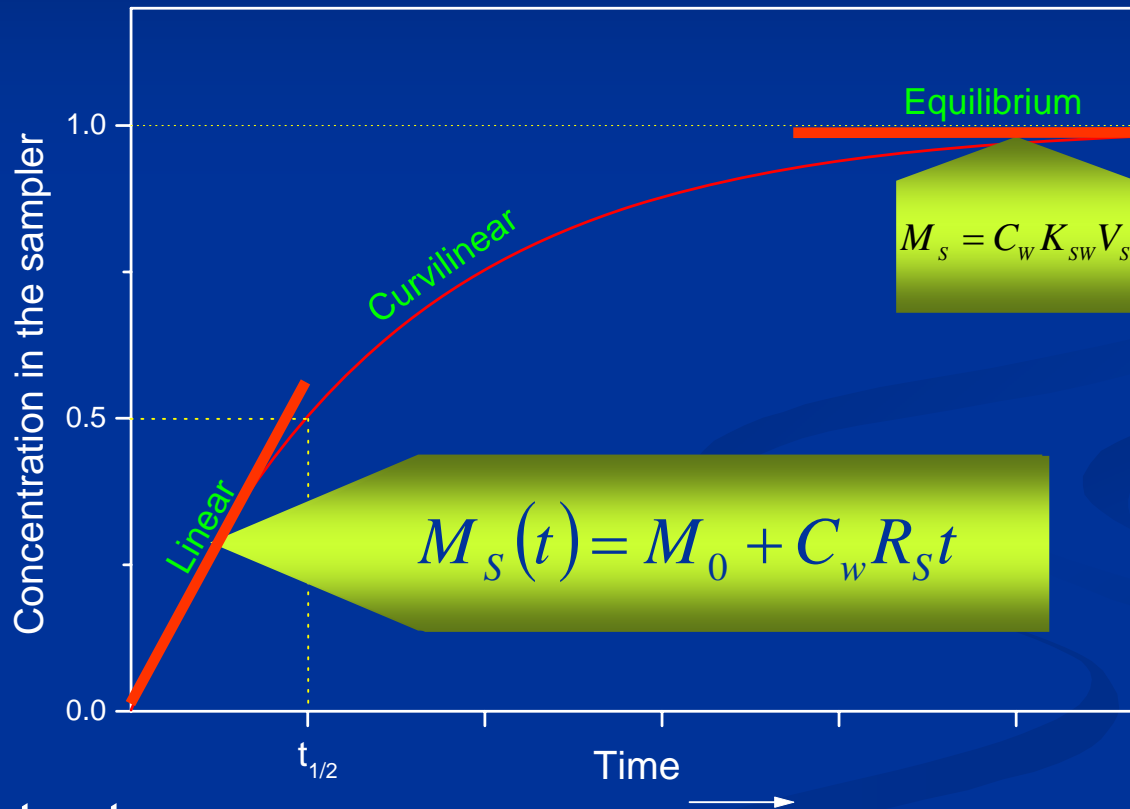
Time weighted average (TWA) sampling

$$C_{TWA} = \frac{C_1 t_1 + C_2 t_2 + C_3 t_3 + \dots + C_n t_n}{t_1 + t_2 + t_3 + \dots + t_n}$$

Principle of a passive sampler



Uptake of a chemical by a passive sampler



$C_w = \text{constant}$

$R_s = \text{substance specific sampling rate [L d}^{-1}\text{]}$



Uptake kinetics of a contaminant into passive sampler

$$C_S(t) = C_{S0} + (C_W K_{SW} - C_{S0}) \left[1 - \exp\left(-\frac{k_o A \alpha}{K_{SW} V_S} t\right) \right]$$

$$C_S(t) = \underbrace{K_{SW} C_W [1 - \exp(-k_e t)]}_{\text{uptake}} + \underbrace{C_{S0} \exp(-k_e t)}_{\text{elimination}}$$

Uptake of a compound to a passive sampler

$$C_S(t) = \underbrace{K_{SW} C_W [1 - \exp(-k_e t)]}_{\text{uptake}} + \underbrace{C_{S0} \exp(-k_e t)}_{\text{elimination}}$$

$C_W \neq 0$ $C_{S0} = 0$: uptake

$$C_S(t) = K_{SW} C_W [1 - \exp(-k_e t)]$$

Elimination of a compound from a passive sampler

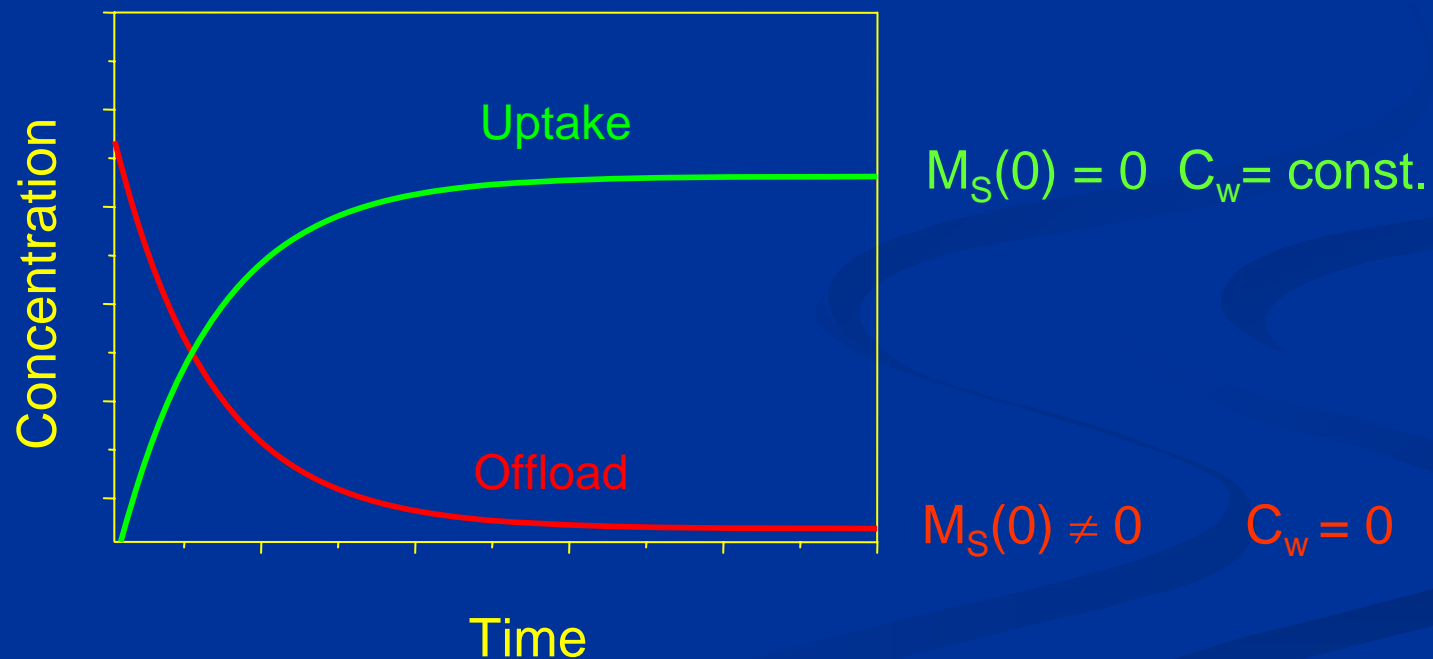
$$C_S(t) = \underbrace{K_{SW} C_W [1 - \exp(-k_e t)]}_{\text{uptake}} + \underbrace{C_{S0} \exp(-k_e t)}_{\text{elimination}}$$

$C_W = 0$ $C_{S0} \neq 0$: only elimination

$$C_S(t) = C_{S0} \exp(-k_e t)$$

Correlation between uptake and offload – PRC concept

In ideal case: both uptake and offload are governed by the same mass transfer law – isotropic exchange kinetics.



Mass transfer in a passive sampler

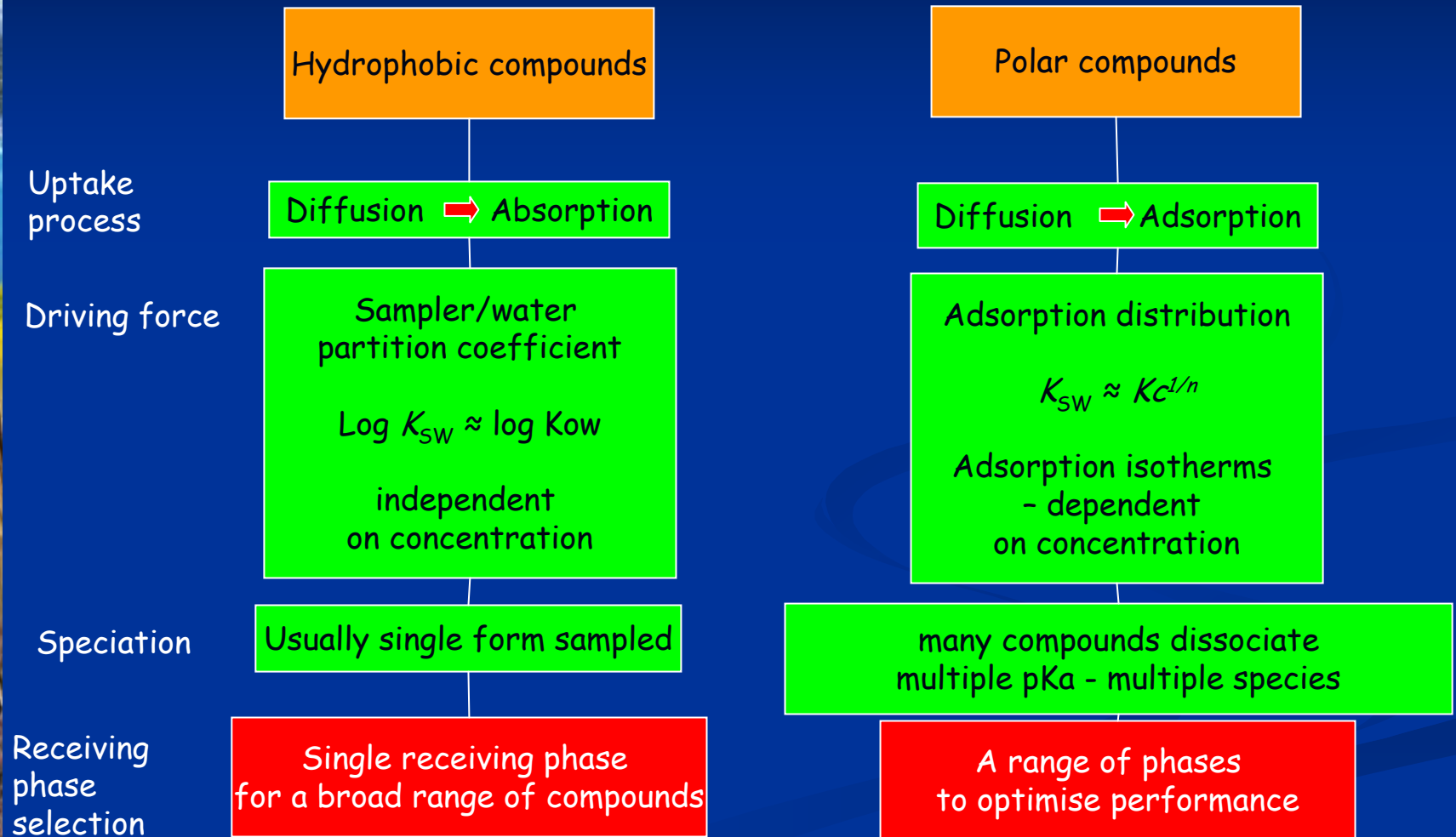
- The overall resistance ($1/k_{ov}$) to the uptake of a chemical into the passive sampler is given by a sum of particular resistances to mass transfer:

$$\frac{1}{k_{ov}} = \sum_i \frac{\delta_i}{K_{iw} D_i} = \frac{\delta_M}{D_M K_{MW}} + \frac{\delta_W}{D_W} + \frac{\delta_S}{D_S K_{SW}}$$

Membrane Water Acceptor

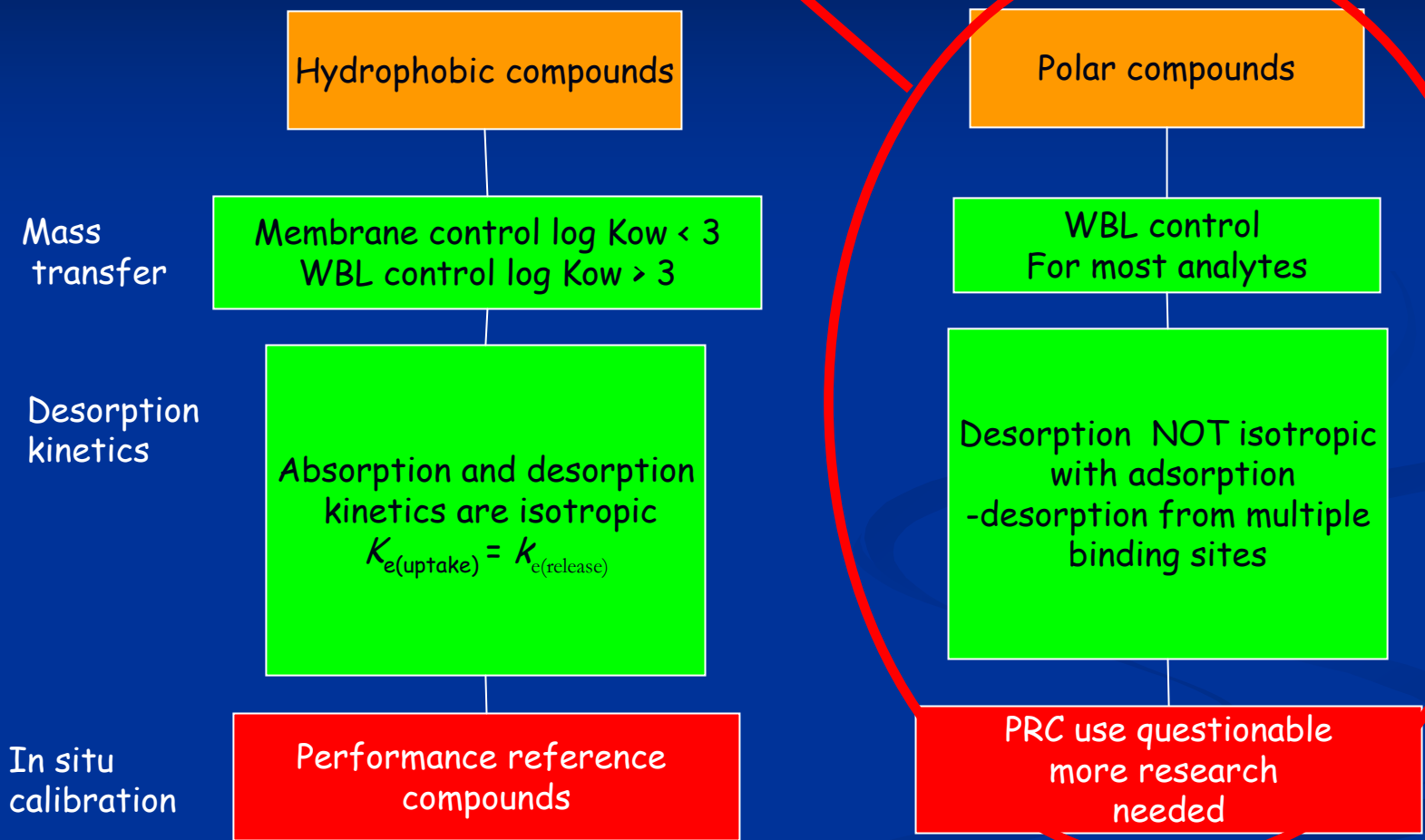
$$k_i = \frac{D_i}{\delta_i}$$

Differences in sampling principles



Differences in sampling principles

Most emerging compounds



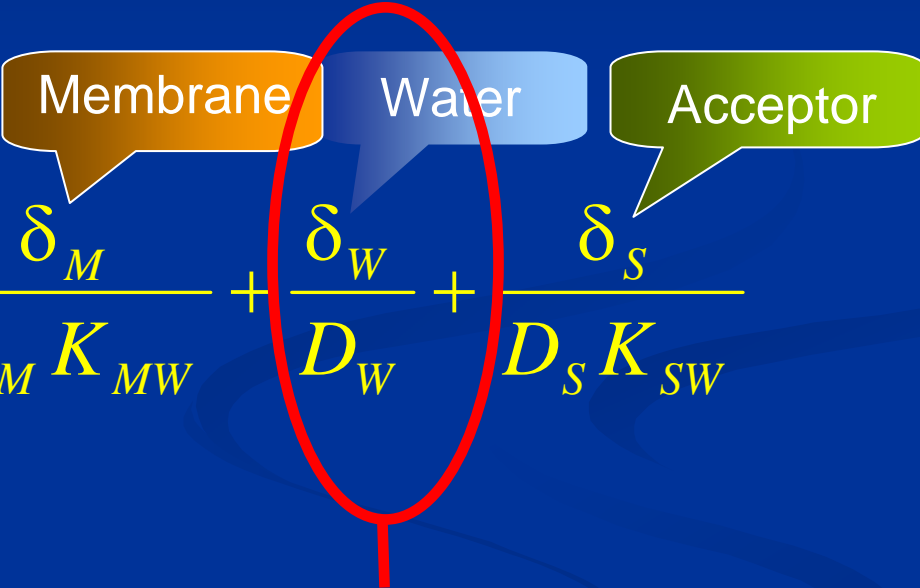
Problems with adsorption based samplers

- Sorption distribution coefficients are not constant, nonlinear adsorption isotherms
- Competitive sorption is likely
- Effect of pH not sufficiently characterised for dissociating compounds
- Absorption is often WBL controlled, thus sampling sensitive to flow turbulence
- Desorption is not isokinetic with adsorption – PRC applicability is questionable

Resistances to Mass transfer in a passive sampler

$$\frac{1}{k_{ov}} = \sum_i \frac{\delta_i}{K_{iw} D_i} = \frac{\delta_M}{D_M K_{MW}} + \frac{\delta_W}{D_W} + \frac{\delta_S}{D_S K_{SW}}$$

Membrane Water Acceptor

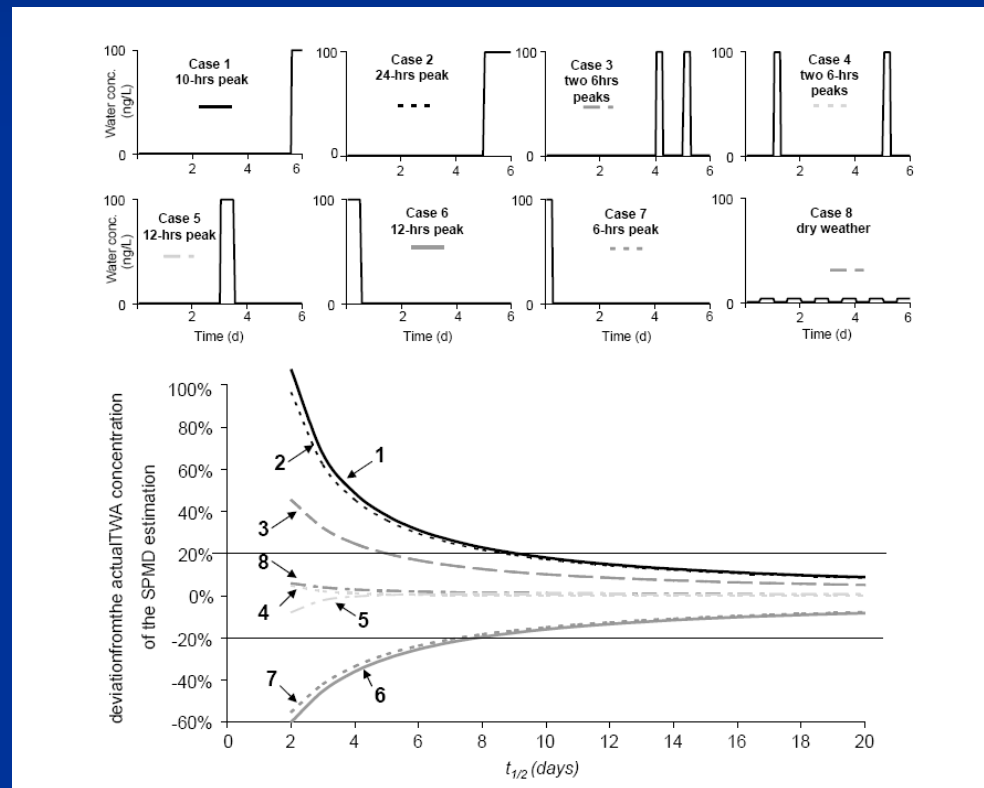


Highly variable resistance

$$k_i = \frac{D_i}{\delta_i}$$

Problems with all samplers

- TWA uncertainty when concentrations fluctuate



C. Gourlay-Francé et al. / Chemosphere 73 (2008) 1194–1200